

Chapter9_example5

The areas are 0.260 sq.ft and 0.287 sq.ft

The raw water flows through the tubes

The equivalent diameter is 0.0444 ft

The Reynolds Number for raw water is 1.66×10^4

The Reynolds Number for distilled water is 1.29×10^4

The Nusselt number for raw water is 97.4

The Nusselt number for distilled water is 123.1

The convective coefficient for raw water based on inner diameter is $618 \text{ BTU}/(\text{hr} \cdot \text{sq} \cdot \text{ft} \cdot \text{degree R})$

The convective coefficient for raw water based on outer diameter is $537 \text{ BTU}/(\text{hr} \cdot \text{sq} \cdot \text{ft} \cdot \text{degree R})$

The convective coefficient for distilled water is $1005 \text{ BTU}/(\text{hr} \cdot \text{sq} \cdot \text{ft} \cdot \text{degree R})$

The overall exchanger coefficient is $350 \text{ BTU}/(\text{hr} \cdot \text{sq} \cdot \text{ft} \cdot \text{degree R})$

The ratio is 0.883 and area is 703.7 sq.ft

$(U_o A_o)/(M_c C_{pc}) = 1.65$

$t_2 = 91.1 \text{ degree F}$

$T_2 = 87.0 \text{ degree F}$

Friction factor for raw water from figure 6.14 corresponding to Reynolds Number calculated above is 0.029

Friction factor for distilled water from figure 6.14 corresponding to Reynolds Number calculated above is 0.281

The velocity of raw water is 2.57 ft/s

The velocity of distilled water is 2.65 ft/s

The pressure drop for tube side is $160.7 \text{ lbf}/\text{sq} \cdot \text{ft} = 1.1 \text{ psi}$

The pressure drop for shell side is $982.4 \text{ lbf/sq.ft} = 6.7 \text{ psi}$

Summary of Requested Information

Outlet Temperatures:

Raw Water: 91.1 degree F

Distilled Water: 87.0 degree F

Pressure Drops:

Raw Water: 1.1 degree F

Distilled Water: 6.7 degree F