

## Chapter9\_example4

The area of annulus is  $2.59 \times 10^{-3}$  sq.m

The area of inner pipe is  $4.28 \times 10^{-3}$  sq.m

Air flows through inner pipe

The heat transferred is  $1.68 \times 10^3$  W

The low temperature of carbon dioxide is 533 K

The LMTD for counter flow configuration is 243 degree C

The Annulus Equivalent Diameter for friction is 0.01862 m

The Annulus Equivalent Diameter for heat transfer is 0.0416 m

The Reynolds Number for air is  $2.42 \times 10^4$

The Reynolds Number for carbon dioxide is  $1.72 \times 10^4$

The Nusselt number for air is 66.5

The Nusselt number for carbon dioxide is 48.9

The convective coefficient for air based on inner diameter is  $25.3 \text{ W}/(\text{sq.m.K})$

The convective coefficient for air based on outer diameter is  $23.6 \text{ W}/(\text{sq.m.K})$

The convective coefficient for carbon dioxide is  $39.4 \text{ W}/(\text{sq.m.K})$

The overall exchanger coefficient is  $14.2 \text{ W}/(\text{sq.m.K})$

The area required is 0.48 sq.m

The number of exchangers is 1

The velocity of air is 5.96 m/s

The velocity of carbon dioxide is 8.98 m/s

The pressure drop for tube side is 12.83 Pa

The pressure drop for shell side is 196 Pa

### Summary of Requested Information

(a) Exchanger required: 1

(b) Overall exchanger coefficient =  $14.2 \text{ W}/(\text{sq.m.K})$

(c) Air pressure drop =  $12.83 \text{ Pa}$

Diesel exhaust pressure drop =  $196 \text{ Pa}$